# Effect of Polymerization Temperature on Propylene Polymerization with C<sub>s</sub>-symmetric Metallocene Catalyst

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**Abstract:** A novel highly active  $C_s$ -symmetric metallocene catalyst namely: *meso*-dimethylsilylbis (2,4,6-trimethyl-1-indenyl)zirconium dichloride is presented. The effect of polymerization temperature (0-70 °C) on the catalyst performance for propylene polymerization has been investigated. This catalyst shows very high activity at 50 °C which is higher than the activity of the racemic analogue, and the resulted polypropylene is amorphous in nature with isotactic pentad content [mmmm] of 12 %.

Keywords: Polymerization, metallocene catalyst, propylene.

The synthesis of bridged ansa metallocenes usually gives a diastereomeric mixture of racemic and meso metallocene isomers and in many cases the meso form is about 50 % of the product of metallocene synthesis<sup>1,2</sup>. The amount of desired racemic isomer is rather poor and can be separated from the meso isomer by fractional crystallization<sup>3</sup>. The racemic *ansa*-metallocene isomer acts as catalyst for propylene polymerization to produce isotactic polypropylene (PP) while the corresponding meso isomer gives atactic PP due to its lack of stereoselectivity<sup>4</sup>. The meso isomer is considered as unwanted product due to its low activity and low molecular weight of the polymer. Collins *et al.* separated the racemic and meso isomer of ethylene bis(tetrahydroindenyl)zirconium dichloride<sup>5</sup>. The pure meso isomer of this complex, when activated with MAO, produced atactic PP at 40 °C with molecular weight (M<sub>w</sub>) of about 2400, at activity of 630 kg-PP/mol-Zr<sup>5</sup>.

We synthesized a novel bridged *ansa*-metallocene catalyst, namely, dimethylsilylbis (2,4,6-trimethyl -1-indenyl) zirconium dichloride and separated its meso and racemic forms by fractional crystallization. The influence of  $T_p$  on the meso isomer of this catalyst for propylene polymerization is reported.

#### **Experimental**

Methylaluminoxane (10 wt.-% toluene solution, Albemarle Co.) was used as received. Toluene was refluxed over Na-benzophenone ketyl under nitrogen atmosphere before use. All procedures in the synthesis, purification of zirconocenes and polymerization process were carried out in argon atmosphere using the Schlenk techniques. Ligand of the zirconocene was synthesized by the method reported in our previous work<sup>6</sup>.

Zhi Qiang FAN et al.

Polymerization grade propylene was further purified by passing it through a column containing supported MnO and over activated 4A molecular sieve column.

The polymerization of propylene was carried out in a 250 mL glass reactor equipped with propylene inlet and magnetic stirrer. After the reactor was flushed with argon, toluene (100 mL) was injected into the reactor with a syringe at required temperature followed by introducing propylene gas to saturate the solvent and maintain at constant pressure of 0.1 MPa. Appropriate amount of MAO was added to the reactor and polymerization was initiated by adding the solution of metallocene in toluene.

<sup>13</sup>C NMR spectra of the polymer were recorded on a Bruker dmx-500 spectrometer at 120°C. The polymer solution (15 wt.-%) was prepared in *o*-dichlorobenzene-d<sub>4</sub>. The intrinsic viscosity of the polymer was determined in decalin as solvent at 135 °C using Ubbelohde viscometer and the molecular weight (M<sub>w</sub>) were calculated by the following equation <sup>7</sup>: [η] = 1.1 x 10<sup>-4</sup> [M<sub>w</sub>]<sup>0.8</sup>.

## **Results and Discussion**

A mixture of racemic and meso forms of the bridged  $\pi$ -ligand substituted zirconocene was obtained from the reaction of dilithio salt of the ligand (I) with ZrCl<sub>4</sub> in CH<sub>2</sub>Cl<sub>2</sub> (Scheme 1). The pure meso form (*meso*-**II**) and pure racemic form (*rac*-**II**) was obtained by fractional crystallization from toluene<sup>8</sup>.

The effect of polymerization temperature T<sub>p</sub> on the polymerization behaviors of meso-II is shown in Table 1. The catalyst activity was very sensitive to the change of T<sub>p</sub>. It increases as the T<sub>p</sub> increases and the maximum activity is obtained at 50 °C. The activity is higher than the activity obtained by the corresponding racemic isomer. In the study of similar zirconocenes for propylene polymerization, Kaminsky et al<sup>9</sup>. and Spaleck et al<sup>-1</sup>. reported that the meso-zirconocene showed much lower activity than the corresponding racemic isomer. For example, propylene polymerization activity by meso-Me<sub>2</sub>Si(2-Me-4,6-*i*-Pr<sub>2</sub>Ind)<sub>2</sub>ZrCl<sub>2</sub> was only 6.4 % of the activity by the racemic zirconocene<sup>9</sup>. The molecular weight of PP by the meso catalyst was also found to be much lower than PP by the racemic one. Other zirconocenes which show such differences between the meso- and rac-isomer include: Me<sub>2</sub>Si(Ind)<sub>2</sub>ZrCl<sub>2</sub>, Me<sub>2</sub>Si(2-MeInd)<sub>2</sub>ZrCl<sub>2</sub>, Me<sub>2</sub>Si(2-Me-4-*i*-PrInd)<sub>2</sub>ZrCl<sub>2</sub> and Me<sub>2</sub>Si(2-Me-4-NaphInd)<sub>2</sub> ZrCl<sub>2</sub>. Therefore, the relatively high polymerization activity and polymer molecular weight observed for the *meso*-II is quite unusual. This phenomenon may be the result of the basically symmetrical spacial arrangement of the methyl groups at 2- and 6-positions of the ligand around the central metal. A detailed molecular mechanics analysis of the catalysis may provide more definite evidences. As indicated by Spaleck *et al.*<sup>1</sup>, the behaviors of *ansa*-metallocene as polymerization catalyst can not be rationally explained in many cases. This may mean that we need to find out those more subtle factors in the structure of metallocene and in the catalysis process, which play important role in special cases. Such work may result in surprising improvement of the catalysts.

## Effect of Temperature on Propylene Polymerization with Cs-symmetric 169 Metallocene Catalyst

Table 1. Effect of polymerization temperature T<sub>P</sub> on catalytic activity and polymer properties

Cat	T <sub>p</sub>	[Zr]	Yield	Activity <sup>a)</sup>	$M_{w}$	T <sub>m</sub> <sup>b)</sup>	mmmm <sup>c)</sup>
	(°C)	µmol/L	(g)		$(x \ 10^{-3})$	(°C)	
meso-II	0	40	0.20	50.0	48.1	amorphous	_ <sup>d)</sup>
meso-II	20	40	1.01	252.5	45.1	amorphous	_ <sup>d)</sup>
meso-II	30	40	1.61	402.5	25.3	amorphous	8.9
meso-II	50	40	17.32	4330.0	17.9	amorphous	13.2
meso-II	70	40	12.18	3045.0	10.6	amorphous	12.1
rac-II	50	20	6.28	3141.0	20.2	146	91.0
rac-II	70	20	8.20	4100.0	12.8	128	71.3

Polymerization conditions: toluene = 100 mL; Al/Zr = 2000; time = 1 h;

 a) in kg-PP/mol-Zr.h ; b) measured by DSC; c) determined by <sup>13</sup>C NMR spectroscopy; d) not measured.

Polypropylene obtained by *meso*-**II** is basically stereorandom at all  $T_p$ . The methyl pentad distribution of PP produced by *meso*-**II** is summarized in **Table 2**. It can be concluded from the pentad intensities at 50 °C that the polymer propagation is controlled by the chain-end control model (4[mm][rr]/[mr]<sup>2</sup> = 1.07) than to the enantiomorphic-site control model (2[rr]/[mr] = 0.78). The heterotactic triad population is [mr] = ~0.50, for perfectly random statistics.

Table 2. Methyl pentad distribution of polypropylene

			mmmm	rinnir	mmrr	xmrx	mrmr	rrrr	mrrr	mrrm
meso-II	30	8.9	13.0	7.8	11.6	23.7	14.2	4.3	10.5	6.0
meso-II	50	13.2	12.8	7.0	10.9	23.6	13.6	4.2	8.6	6.0
meso-II	70	12.1	12.1	6.5	12.2	23.5	12.6	5.2	9.8	6.1
rac-II	50	91	3.6	0	2.5	1.6	0.7	0	0	0.5

Polymerization conditions are the same as in table 1, xmrx = mmrm + rmrr

The polymer obtained at 50 °C was extracted by refluxing diethyl ether and 18.8 wt % of the polymer was insoluble. The <sup>13</sup>C NMR spectrum of the diethyl ether insoluble fraction has the methyl pentad distributions [mmmm] = 42.6, [mmmr] = 11.0, [rmmr] = 4.5, [mmrr] = 7.9, [mmrm] + [rmrr] = 13.9, [mrmr] = 7.8, [rrrr] = 2.8, [mrrr] = 6.3, [mrrm] = 3.1, the triad population of [mm] = 58.1, [mr] = 29.6 and [rr] = 21.2 while the M<sub>w</sub> is 31.9 x 10<sup>-3</sup> and T<sub>m</sub> is 137.9 °C. The polymer obtained at T<sub>p</sub> = 50 °C was also extracted with boiling heptane and gave 98.4 % heptane soluble fraction and only 1.6 % heptane insoluble fraction.

Moreover, all the samples obtained by *meso*-**II** at different  $T_p$  contained no regioirregularity due to 2,1- or 1,3-insertion as compared to the polymer obtained with its corresponding *rac*-**II** isomer which contains 0.42 % 2,1-insertion and 0.17 % 1,3-insertion.

In conclusion, the activity of *meso*-**II** for propylene polymerization has been found to be very sensitive to polymerization temperature. Very high activity was observed at 50 °C and higher temperature, which is even higher than the activity of the corresponding racanalogue. The polymer molecular weight by *meso*-**II** was also not much different from that by *rac*-**II**. This is a novel phenomenon different from similar systems reported in literature. High activity and polymer molecular weight make the *meso*-**II** a potentially practical catalyst for producing atactic-PP.

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